HOW THE POLARITY OF A SURFACE REACTING WITH A LOW-TEMPERATURE PLASMA AFFECTS THE THERMODYNAMIC VARIABLES IN METALLURGICAL REACTIONS')

V. DEMBOVSKݲ), Ostrava

on the assumption that this plasma is in thermodynamic equilibrium state and that its composition is known. A positive polarity of the reacting surface is shown to reduce the thermodynamic probability of the desired reaction taking place. A negatively charged which attend heterogeneous metallurgical reactions involving a low-temperature plasma, reacting surface are not absolutely accurate. They are, however, accurate enough for all thermal boundary layer, the equations derived for the particle flow densities at the stable oxides. As the following expressions neglect the recombination processes in the reacting surface allows metals to be gained by the hydrogen reduction of even extremely practical purposes. Reactionships are presented for calculating the changes in thermodynamic variables

НА ТЕРМОДИНАМИЧЕСКИЕ ПЕРЕМЕННЫЕ В МЕТАЛЛУРГИЧЕСКИХ КАКОЕ ВЛИЯНИЕ ОКАЗЫВАЕТ ПОЛЯРНОСТЬ ПОВЕРХНОСТИ, РЕАГИРУЮЩЕЙ С НИЗКОТЕМПЕРАТУРНОЙ ПЛАЗМОЙ, РЕАКЦИЯХ

переменных, которые сопровождают гетерогенные металлургические реакции с низкотемпературной плазмой, в предположении, что плазма находится в терслое, уравнения, выведенные для плотностей потока частиц на реагирующей восстановления водородом даже особо устойчивые окиси. Поскольку данные заряженная поверхность допускает, чтобы металлы приобретали при помощи положительная полярность реагирующей поверхности уменьшает термодинамическом равновесном состоянии и что ее состав известен. Показано, что поверхности, не являются абсолютно точными. Их точность, однако, достаточна выражения пренебрегают процессами рекомбинации в термическом граничном для всех практических целей. модинамическую вероятность происхождения данной реакции. Отрицательно В работе приведены соотношения для расчета изменений термодинамических

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²) College of Mining and Metallurgy, 708 33 OSTRAVA, Czechoslovakia

I. PHYSICAL INTERACTIONS OF ACTIVE PARTICLES IN THE ABSENCE OF AN EXTERNALLY APPLIED ELECTRIC FIELD

The basic metallurgical reactions exploited for extractive and refining processes take place predominantly in heterogeneous systems. In a heterogeneous system incorporating a plasma, the component in the plasma state is generally the extracting or refining medium, while the processed material is in the solid or liquid

The density of the flow of active particles of the jth kind, reaching an electrically insulated surface that is in contact with the plasma stream, is given by a generalized

$$\psi_i = \frac{n_i v_{s,i}}{4} \tag{1}$$

where n_i is the concentration of particles of this *j*th kind in the surrounding plasma stream, $v_{s,j}$ is the arithmetic mean velocity of the *j*th kind.

After substituting the numerical values of the constants in the formula describing the arithmetic mean velocity of the particles,

$$v_{s,j} = \left(\frac{8kT_j}{\pi m_j}\right)^{1/2} = 5.93 \times 10^{-12} \left(\frac{T_j}{m_j}\right)^{1/2}$$
 (2)

where k is the Boltzmann constant $(1.38054 \times 10^{-23} \text{ JK}^{-1})$, T_i is the ther-

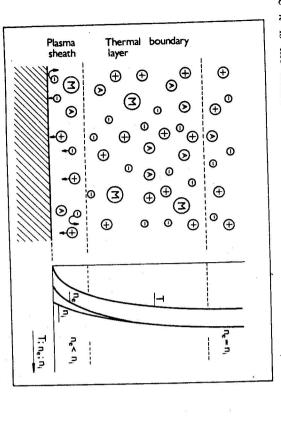


Fig. 1. Scheme of the transport of active particles from a lowtemperature plasma to the reacting surface in the absence of an applied electric field.

modynamic temperature of particles of the jth kind, and m_i is the mass of particles of the j-th kind, and inserting the resultant expression into equation (1), we obtain a formula better suited for routine calculations:

$$\psi_i = 1.48 \times 10^{-12} n_i \left(\frac{T_i}{m_i}\right)^{1/2} \qquad [\text{m}^{-2} \text{s}^{-1}]$$
 (3)

A scheme of a heterogeneous system in the absence of an externally applied electric field, showing the transport of active particles from the plasma to the surface of the processed material, is presented in Fig. 1.

II. HETEROGENEOUS SYSTEMS IN THE PRESENCE OF AN APPLIED ELECTRIC FIELD

When the electrically conductive charged surface is incorporated in the plasma torch circuit, or when a voltage is applied across this surface and the plasma stream, the situation arising conforms essentially to the scheme in Figs. 2 or 3, depending on the polarity of the charged surface.

When the surface charge is negative in polarity, the ions that impinge on it deliver a current density J_i which varies with the voltage drop across the collision-free plasma sheat and with the thickness of that sheath [1], as follows:

$$J_{i} = \frac{1}{9\pi} \left(\frac{2e}{m_{i}} \right)^{1/2} \frac{V_{s}^{9/2}}{d_{s}^{2}} \left[1 + 2.66 \left(\frac{kT_{i}}{eV_{s}} \right)^{1/2} \right] \qquad [Am^{-2}]$$
 (4)

where d_s is the thickness of the plasma sheath [m], m_t is the mass of an ion [kg], e is the charge of an electron $(1.60210 \times 10^{-19} \text{ C})$, T_t is the thermodynamic temperature of the ions, and V_s is the voltage drop across the sheath, i.e. within d_s , which in this case corresponds to the anode voltage gradient [V] and is defined as [2]

$$V_s = \frac{1}{2} \frac{kT_e}{e} \ln \left(\frac{2m_e}{\pi m_e} \right). \tag{5}$$

When the surface is negatively charged, the density of the flow of singly ionized positive ions impacting on it is given by

$$\psi_i = \frac{J_i}{e}. \tag{6}$$

In a heterogeneous system where the conductive charged surface forms the cathode the density of the flow of singly ionized ions reaching that solid or liquid surface from the plasma can be established from the relation

$$\frac{I}{s_{e}} - \frac{J_{e}}{e} \tag{7}$$

13

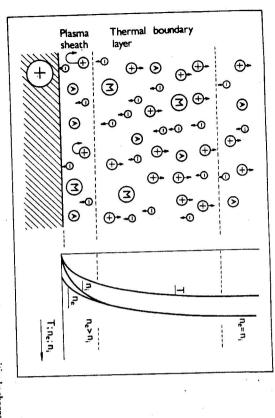


Fig. 2. Scheme of the transport of active particles from a low-temperature plasma to a positively charged reacting surface.

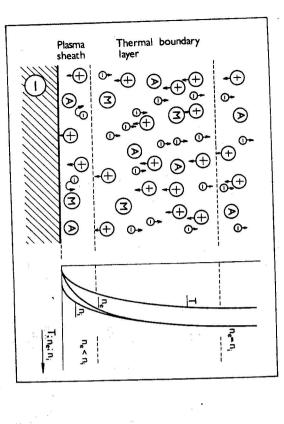


Fig. 3. Scheme of the transport of active particles from a low-temperature plasma to a negatively charged reacting surface.

where I is the discharge current [A], and F_k the active area of the cathode or cathode spot [m²].

III. COMPARISON OF THE THERMODYNAMIC PARAMETERS OF REACTIONS INVOLVING A LOW-TEMPERATURE PLASMA

Let us assume that in a reaction described by

$$B+D_2 \rightarrow C+R$$

the diatomic molecules of substance D₂ enter reaction (8) in the form of a low-temperature plasma made up of molecules, atoms, ions and electrons. This

reaction will then be described by
$$B + xD_2 + 2yD + 2zD^+ + 2ze \rightarrow C + R$$

9

where x, y and z are the molar fractions of particles on the molecular, atomic and ionic states, respectively. If in the course of this reaction the atoms and ions of substance D recombine, then the standard heat of the metallurgical reaction for the process conforming to scheme (9) will be

$$\Delta H^{0} = \left[\Delta H_{C}^{0} + \Delta H_{R}^{0}\right] - \left\{\Delta H_{B}^{0} + x\Delta H_{D_{z}}^{0} + 2y\frac{1}{2}\left(\Delta H_{dis}^{0}\right)_{D_{z}} + \right]$$
(10)

$$+2z\bigg[\frac{1}{2}\left(\Delta H_{\text{dis}}^{0}\right)_{D_{2}}+\left(\Delta H_{\text{ion}}^{0}\right)_{D}\bigg]\bigg\}.$$

The change in standard entropy will be determined by

$$\Delta S^{0} = \left[S_{C}^{0} + S_{R}^{0}\right] - \left\{S_{B}^{0} + xS_{D_{2}}^{0} + 2y\frac{1}{2}\left[S_{D_{2}}^{0} + (\Delta S_{dis}^{0})_{D_{2}}\right] + \right]$$

(11)

$$+2z\bigg[\frac{1}{2}S_{0z}^{0}+\frac{1}{2}(\Delta S_{dis}^{0})_{Dz}+(\Delta S_{ion}^{0})_{D}\bigg]\bigg\}.$$

The change in the standard Helmholtz energy can be ascertained from

$$\Delta \mathbf{F}^{0} = \left[\Delta \mathbf{F}_{C}^{0} + \Delta \mathbf{F}_{R}^{0} \right] - \left\{ \Delta \mathbf{F}_{B}^{0} + x \Delta \mathbf{F}_{D_{2}} + 2y \frac{1}{2} \left(\Delta \mathbf{F}_{dis}^{0} \right)_{D_{2}} + \right.$$

$$\left. + 2z \left[\frac{1}{2} \left(\Delta \mathbf{F}_{dis}^{0} \right)_{D_{2}} + \left(\Delta \mathbf{F}_{ion}^{0} \right)_{D} \right] \right\}.$$

$$(12)$$

The change in the standard Gibbs energy caused by the metallurgucal reaction will

$$\Delta G^{0} = \left[\Delta G_{C}^{0} + \Delta G_{R}^{0}\right] - \left\{\Delta G_{B}^{0} + x\Delta G_{D_{2}}^{0} + 2y\frac{1}{2}\left(\Delta G_{dis}^{0}\right)_{D_{2}} + \right.$$
(13)

$$+2z\bigg[\frac{1}{2}\left(\Delta G_{dis}^{0}\right)_{D_{2}}+\left(\Delta G_{ion}^{0}\right)_{D}\bigg]\bigg\}$$

tively, of substance D which participe in this reaction. The general definition of the size of any molar fraction is n_{D_2} , n_D and n_{D^+} being the concentrations of molecules, atoms and ions, respec $x = \frac{1}{n_{D_2} + n_D + n_{D^+}}; \quad y = \frac{1}{n_{D_2} + n_D + n_{D^+}}; \quad z = \frac{1}{n_{D_2} + n_D + n_D + n_{D^+}}; \quad z = \frac{1}{n_{D_2} + n_D + n_D$

 $n_{\mathrm{D_2}} + n_{\mathrm{D}} + n_{\mathrm{D}}$

$$x, y, z = \frac{n_i}{\sum_{n_i}} \tag{14}$$

molar fraction of the various particle kinds which constitute the plasma are far that participate in the reaction. When we deal with plasma processes, however, the where n_i is the concentration (particle number density) of particles of the jth kind product of two variables; the concentration of those particles, n_i , and their better expressed in terms of the particle flow densities on the reacting surface arithmetic mean velocity, $v_{s,i}$. Upon inserting the expanded expression for the Equation (1) shows that the density of a particle flow is directly proportional to the particle concentration obtained from formula (1),

$$n_i = 4\psi_i \left(\frac{\pi m_i}{8kT_i}\right)^{1/2} \tag{15}$$

into formula (14), we can set up an equation for calculating the molar fractions of various kinds of reacting particles in terms of the particle flow densities:

$$x, y, z = \frac{\psi_i(m_i)^{1/2}}{\sum_i \psi_i(m_i)^{1/2}}$$
(16)

which they react. For the reaction described by scheme (9) we can thus formulate where $\Sigma_i \psi_i$ is the total density of all the reacting particle flows on the surface with the molar fractions of the various reacting particle kinds as follows:

$$x = \frac{\psi_{D_2}(m_{D_2})^{1/2}}{\psi_{D_2}(m_{D_2})^{1/2} + \psi_{D}(m_{D})^{1/2} + \psi_{D^*}(m_{D^*})^{1/2}}$$

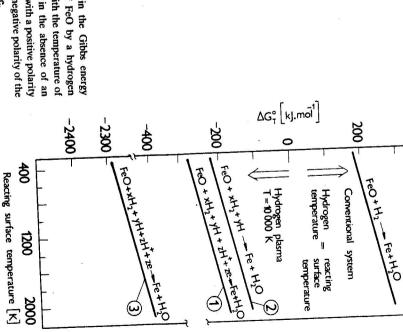
$$y = \frac{\psi_{D_2}(m_{D_2})^{1/2} + \psi_{D}(m_{D})^{1/2}}{\psi_{D^*}(m_{D^*})^{1/2} + \psi_{D^*}(m_{D^*})^{1/2}}$$

$$z = \frac{\psi_{D_2}(m_{D_2})^{1/2} + \psi_{D}(m_{D})^{1/2} + \psi_{D^*}(m_{D^*})^{1/2}}{\psi_{D^*}(m_{D_2})^{1/2} + \psi_{D}(m_{D})^{1/2} + \psi_{D^*}(m_{D^*})^{1/2}}.$$
(17)

and temperatures. Under such conditions their termodynamic probability is In practice most metallurgical reactions take place at roughly constant pressures

16

change is, e.e. the greater the decrement in the Gibbs energy. The course of these governed by the attendant changes in the Gibbs energy: a metallurgical reaction computed by the conventional procedure with the aid of the Gibbs-Helmholtz changes, in dependence on the temperature of the reacting system, can be will proceed the more completely and perfectly, the more negative the value of the



attending the reduction of FeO by a hydrogen plasma at 10 000 K vary with the temperature of Fig. 4. How the changes in the Gibbs energy of the surface; 3 — with a negative polarity of the applied electric field; 2 — with a positive polarity the reacting surface: 1 - in the absence of an

at 10 000 K, in a reaction described by reacting surface of solid iron oxide when the latter is reduced by a hydrogen plasma Fig. 4 shows the changes in the Gibbs energy at various temperatures of the

$$FeO + xH_2 + 2yH + 2zH^+ + 2ze \rightarrow Fe + H_2O.$$
 (20)

paper, show that a positive polarity of the reacting surface reduces the ther-The changes in the Gibbs energy, ascertained by the techniques outlined in this

modynamic polarity of this reaction, as against the state when no external electric field was applied. In the extreme case of a fully ionized hydrogen plasma, Fig. 2 reduction with a hydrogen plasma will permit metals to be gained even from highly probability increment suggests that, given a negatively charged reacting surface, interactions with the FeO surface, so that no reaction will take place. This indicates that a situation may arise where no hydrogen particles will participate in stable oxides.

REFERENCES

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